

Partial Differential Equations

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Functions of More Than One Variable

- Almost all processes relevant in geosciences are described by variables varying in time and space. The spatial component is a scalar in case of a one-dimensional description and a vector in case of a two- or three-dimensional description.

Examples:

$T(\vec{x}, t)$ as the temperature

$\rho(\vec{x}, t)$ as the fluid pressure in a reservoir

$\rho(\vec{x}, t)$ as the density in a gas

$\vec{v}(\vec{x}, t)$ as the flow velocity in a fluid

- Spatial interactions often refer to the spatial variation in the variables.

Examples:

Heat conduction is driven by spatial differences in temperature.

Fluid flow is driven by spatial differences in pressure.

Partial Derivatives

- If a function u depends on more than one variable, e. g., $u(x_1, x_2, x_3, t)$ (or shorter $u(\vec{x}, t)$), the derivative with respect to one of the variables (while the others are constant) is called **partial derivative**.
- Partial derivatives are written with the symbol ∂ , e. g.,

$$\frac{\partial}{\partial x_1} u(\vec{x}, t), \quad \frac{\partial}{\partial x_2} u(\vec{x}, t), \quad \frac{\partial}{\partial x_3} u(\vec{x}, t), \quad \text{and} \quad \frac{\partial}{\partial t} u(\vec{x}, t).$$

- Partial derivatives are computed by assuming that the other variables are constant.

Examples of Partial Derivatives

- Density of an ideal gas

$$\rho(p, T) = \frac{M}{R} \frac{p}{T} \quad \text{with} \quad \begin{array}{l} M = \text{molar mass} \\ R = \text{gas constant} \end{array}$$

$$\frac{\partial}{\partial p} \rho(p, T) = \quad , \quad \frac{\partial}{\partial T} \rho(p, T) =$$

- One-dimensional harmonic wave

$$u(x, t) = A \sin(\omega t - kx) \quad \text{with} \quad \begin{array}{l} A = \text{amplitude} \\ \omega = \text{angular frequency} \\ k = \text{wave number} \end{array}$$

$$\frac{\partial}{\partial x} u(x, t) = \quad , \quad \frac{\partial}{\partial t} u(x, t) =$$

The Gradient

The partial derivatives with respect to the spatial coordinates are often subsumed in a vector

$$\operatorname{grad} u(\vec{x}, t) = \nabla u(\vec{x}, t) = \begin{pmatrix} \frac{\partial}{\partial x_1} u(\vec{x}, t) \\ \frac{\partial}{\partial x_2} u(\vec{x}, t) \\ \frac{\partial}{\partial x_3} u(\vec{x}, t) \end{pmatrix}$$

Examples:

$$H(x_1, x_2) = x_1^2 - x_2^2, \quad \nabla H(x_1, x_2) = \begin{pmatrix} \\ \end{pmatrix}$$

$$H(x_1, x_2) = x_1 x_2, \quad \nabla H(x_1, x_2) = \begin{pmatrix} \\ \end{pmatrix}$$

Properties of the Gradient

- $\nabla u(\vec{x})$ is normal to the lines (in 2D) or the surfaces (in 3D) where $u(\vec{x})$ is constant.
- $\nabla u(\vec{x})$ points in direction of steepest increase of $u(\vec{x})$.
- The length of $\nabla u(\vec{x})$ is the slope of $u(\vec{x})$ in direction of steepest increase.

What Is a Partial Differential Equation?

A **partial differential equation** (PDE) is an equation for an unknown function depending on more than variable involving partial derivatives.

A differential equation for a function of only one variable is called **ordinary differential equation** (ODE).

The One-Dimensional Advection Equation

$$\frac{\partial}{\partial t} u(x, t) = -v \frac{\partial}{\partial x} u(x, t)$$

The Equation of Continuity (mass conservation) in a Fluid

$$\begin{aligned} \frac{\partial}{\partial t} \rho(\vec{x}, t) &= -\operatorname{div}(\rho(\vec{x}, t) \vec{v}(\vec{x}, t)) \\ &= -\frac{\partial}{\partial x_1} (\rho(\vec{x}, t) v_1(\vec{x}, t)) - \frac{\partial}{\partial x_2} (\rho(\vec{x}, t) v_2(\vec{x}, t)) \\ &\quad - \frac{\partial}{\partial x_3} (\rho(\vec{x}, t) v_3(\vec{x}, t)) \end{aligned}$$

The Heat Conduction Equation

Simplest version (1D with constant parameters):

$$\frac{\partial}{\partial t} T(x, t) = \kappa \frac{\partial^2}{\partial x^2} T(x, t)$$

General version (3D):

$$\begin{aligned} \rho c \frac{\partial}{\partial t} T(\vec{x}, t) &= \operatorname{div}(\lambda \nabla T(\vec{x}, t)) \\ &= \frac{\partial}{\partial x_1} \left(\lambda \frac{\partial}{\partial x_1} T(\vec{x}, t) \right) + \frac{\partial}{\partial x_2} \left(\lambda \frac{\partial}{\partial x_2} T(\vec{x}, t) \right) \\ &\quad + \frac{\partial}{\partial x_3} \left(\lambda \frac{\partial}{\partial x_3} T(\vec{x}, t) \right) \end{aligned}$$

The Navier-Stokes Equations of a Viscous Fluid (without gravity)

$$\rho \left(\frac{\partial}{\partial t} \vec{v}(\vec{x}, t) + (\vec{v}(\vec{x}, t) \cdot \nabla) \vec{v}(\vec{x}, t) \right) = -\nabla p(\vec{x}, t) + \eta \Delta \vec{v}(\vec{x}, t)$$

with

$$\begin{aligned} (\vec{v}(\vec{x}, t) \cdot \nabla) \vec{v}(\vec{x}, t) &= v_1(\vec{x}, t) \frac{\partial}{\partial x_1} \vec{v}(\vec{x}, t) + v_2(\vec{x}, t) \frac{\partial}{\partial x_2} \vec{v}(\vec{x}, t) \\ &\quad + v_3(\vec{x}, t) \frac{\partial}{\partial x_3} \vec{v}(\vec{x}, t) \\ \Delta \vec{v}(\vec{x}, t) &= \frac{\partial^2}{\partial x_1^2} \vec{v}(\vec{x}, t) + \frac{\partial^2}{\partial x_2^2} \vec{v}(\vec{x}, t) + \frac{\partial^2}{\partial x_3^2} \vec{v}(\vec{x}, t) \end{aligned}$$

Treatment of the Time Coordinate

The procedure is basically the same as for the time in ordinary differential equations:

- If second-order derivatives occur, the first-order derivatives must be introduced as separate variables.
- Approximate solutions are computed step by step (in steps of length δt), starting from the initial time t_0 .
- The time derivative is approximated by

$$\frac{\partial}{\partial t} u(\vec{x}, t) \approx \frac{u(\vec{x}, t + \delta t) - u(\vec{x}, t)}{\delta t}.$$

Treatment of the Time Coordinate

- All schemes (explicit and fully implicit Euler, mixed, e. g., Crank-Nicholson) can be used.
- If the explicit Euler scheme is used, the solution $u(\vec{x}, t + \delta t)$ can be directly obtained from $u(\vec{x}, t)$ by computing partial derivatives of $u(\vec{x}, t)$ with respect to the spatial coordinates \vec{x} .
- For all implicit schemes, a partial differential equation with respect to the spatial coordinates \vec{x} remains to be solved in each timestep.

The Finite-Difference Method in One Dimension

One-dimensional case: only one spatial coordinate x (and time)

First step:

- Discrete points x_1, x_2, \dots, x_n are defined on the considered part of the x -axis (from the left-hand boundary to the right-hand boundary).
- These points are called **nodes** and are the points where an approximate solution will be computed.
- The nodes may be equidistant (having all the same distance δx) or not.

The Finite-Difference Method in One Dimension

Second step: The partial derivatives $\frac{\partial}{\partial x} u(x, t)$ are approximated by difference quotients.

Right-handed difference quotient:

$$\frac{\partial}{\partial x} u(x, t) \approx \frac{u(x + \delta x, t) - u(x, t)}{\delta x}$$

Left-handed difference quotient:

$$\frac{\partial}{\partial x} u(x, t) \approx \frac{u(x, t) - u(x - \delta x, t)}{\delta x}$$

The Finite-Difference Method in One Dimension

Central (symmetric) difference quotient:

$$\frac{\partial}{\partial x} u(x, t) \approx \frac{u(x + \delta x, t) - u(x - \delta x, t)}{2\delta x}$$

or

$$\frac{\partial}{\partial x} u(x, t) \approx \frac{u(x + \frac{\delta x}{2}, t) - u(x - \frac{\delta x}{2}, t)}{\delta x}$$

or

$$\frac{\partial}{\partial x} u(x + \frac{\delta x}{2}, t) \approx \frac{u(x + \delta x, t) - u(x, t)}{\delta x}$$

or

$$\frac{\partial}{\partial x} u(x - \frac{\delta x}{2}, t) \approx \frac{u(x, t) - u(x - \delta x, t)}{\delta x}$$

Only the first version can be applied directly, the others are only useful for combining them to second-order derivatives.

The Finite-Difference Method in One Dimension

- The accuracy of all these difference quotients decreases with increasing δx .
- As long as there is no preferred direction, right-hand and left-hand difference quotients are equivalent.
- Central difference quotients provide a higher accuracy than the one sided versions.

General Concept

Consider the amount of anything that is worth keeping track of (mass, energy, ...) in a volume

rate of change of the amount stored within the volume

=

amount per time entering at the boundaries

-

amount per time leaving at the boundaries

+

amount per time produced within the volume

-

amount per time removed within the volume

Density and Flux Density

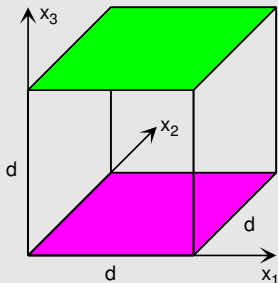
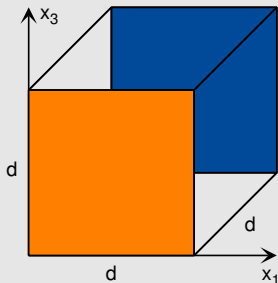
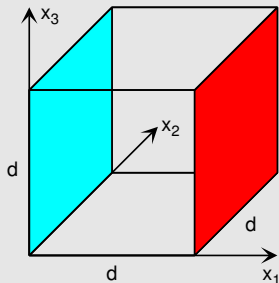
Density $u(\vec{x}, t)$ = amount per volume

Flux density $\vec{q}(\vec{x}, t)$ = amount passing a surface per time and surface area

\vec{q} is a vector, so that the amount per time passing a (small) surface of size A with a unit normal vector \vec{n} is $\vec{q} \cdot \vec{n}A$.

The Equation of Continuity

Balance of a the amount contained in a cube:



$$\frac{\partial u}{\partial t} d^3 = q_1 d^2 - q_1 d^2 + q_2 d^2 - q_2 d^2 + q_3 d^2 - q_3 d^2 + Q d^3$$

where Q is the rate of production (amount per time and volume)

The General Balance Equation

$$\frac{\partial}{\partial t} u(\vec{x}, t) = -\operatorname{div} \vec{q}(\vec{x}, t) + Q(\vec{x}, t)$$

where

$$\begin{aligned} \operatorname{div} \vec{q}(\vec{x}, t) &= \frac{\partial}{\partial x_1} q_1(\vec{x}, t) + \frac{\partial}{\partial x_2} q_2(\vec{x}, t) + \frac{\partial}{\partial x_3} q_3(\vec{x}, t) \\ &= \text{divergence of the flux density } \vec{q} \end{aligned}$$

The Equation of Advection

Assume that the considered amount moves at a given velocity $\vec{v}(\vec{x}, t)$:

$$\vec{q}(\vec{x}, t) = u(\vec{x}, t) \vec{v}(\vec{x}, t)$$



$$\frac{\partial}{\partial t} u(\vec{x}, t) = -\operatorname{div} (u(\vec{x}, t) \vec{v}(\vec{x}, t)) + Q(\vec{x}, t)$$

In 1D:

$$\frac{\partial}{\partial t} u(x, t) = -\frac{\partial}{\partial x} (u(x, t) \vec{v}(x, t)) + Q(x, t)$$

The equation of advection is of first order in both time and space (hyperbolic differential equation).

The Equation of Advection

Simplest version: $\vec{v}(\vec{x}, t) = \text{const.}$, $Q(\vec{x}, t) = 0$:

$$\frac{\partial}{\partial t} u(\vec{x}, t) = -\vec{v} \cdot \nabla u(\vec{x}, t)$$

In 1D:

$$\frac{\partial}{\partial t} u(x, t) = -v \frac{\partial}{\partial x} u(x, t)$$

The Diffusion Equation

- 1 Flux follows the direction of steepest descent of the density $u(\vec{x}, t)$.
- 2 The flux density is proportional to the decrease of density per length.

$$\vec{q}(\vec{x}, t) = -D \nabla u(\vec{x}, t) = -D \begin{pmatrix} \frac{\partial}{\partial x_1} u(\vec{x}, t) \\ \frac{\partial}{\partial x_2} u(\vec{x}, t) \\ \frac{\partial}{\partial x_3} u(\vec{x}, t) \end{pmatrix}$$

with

$$D = \text{diffusivity (coefficient of diffusion)} \left[\frac{\text{m}^2}{\text{s}} \right]$$

The Diffusion Equation

Insert flux density into the balance equation:

$$\begin{aligned}\frac{\partial}{\partial t} u(\vec{x}, t) &= -\operatorname{div} \vec{q}(\vec{x}, t) + Q(\vec{x}, t) \\ &= \operatorname{div} (D \nabla u(\vec{x}, t)) + Q(\vec{x}, t)\end{aligned}$$

In 1D:

$$\frac{\partial}{\partial t} u(x, t) = \frac{\partial}{\partial x} \left(D \frac{\partial}{\partial x} u(x, t) \right) + Q(x, t)$$

The diffusion equation is of first order in time and of second order in space (parabolic differential equation).

The Diffusion Equation

Simplest version: $D = \text{const.}$, $Q(\vec{x}, t) = 0$:

$$\begin{aligned}\frac{\partial}{\partial t} u(\vec{x}, t) &= D \operatorname{div} \nabla u(\vec{x}, t) \\ &= D \left(\frac{\partial^2}{\partial x_1^2} u(\vec{x}, t) + \frac{\partial^2}{\partial x_2^2} u(\vec{x}, t) + \frac{\partial^2}{\partial x_3^2} u(\vec{x}, t) \right) \\ &= D \Delta u(\vec{x}, t)\end{aligned}$$

where $\Delta = \frac{\partial^2}{\partial x_1^2} + \frac{\partial^2}{\partial x_2^2} + \frac{\partial^2}{\partial x_3^2}$ is the **Laplace operator**.

In 1D:

$$\frac{\partial}{\partial t} u(\vec{x}, t) = D \frac{\partial^2}{\partial x^2} u(x, t)$$

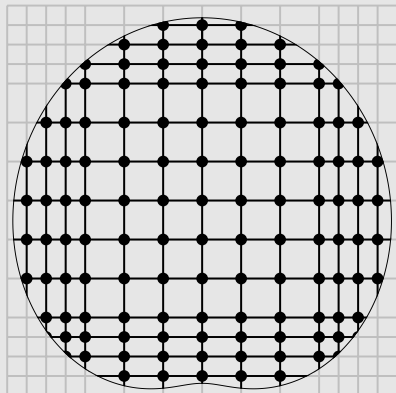
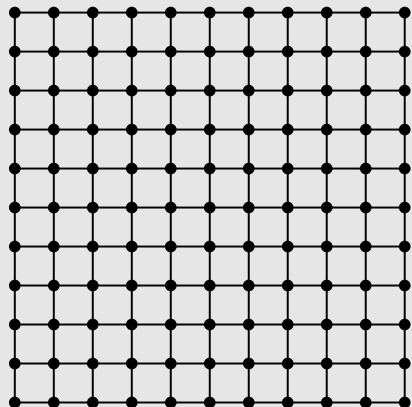
Initial Conditions and Boundary Conditions

- Time is distinct from the spatial coordinates as it is directed.
- For a unique solution, partial differential equations require
 - Initial conditions:** The solution for all points \vec{x} of the domain at a time t_0 must be given.
 - Boundary conditions:** The solution (or, e. g., its derivatives) must be given at (least at a part of) the boundary of the domain for all times $t > t_0$.

The Finite-Difference Method in Two Dimensions

Two-dimensional case: Spatial coordinates x_1 and x_2 .

First step: The domain is covered by a lattice where the lines are parallel to the coordinate axes.



The Finite-Difference Method in Two Dimensions

Second step: The partial derivatives $\frac{\partial}{\partial x_1} u(x, t)$ and $\frac{\partial}{\partial x_2} u(x, t)$ are approximated by difference quotients.

Right-handed difference quotients:

$$\frac{\partial}{\partial x_1} u(x_1, x_2, t) \approx \frac{u(x_1 + \delta x, x_2, t) - u(x_1, x_2, t)}{\delta x}$$

$$\frac{\partial}{\partial x_2} u(x_1, x_2, t) \approx \frac{u(x_1, x_2 + \delta x, t) - u(x_1, x_2, t)}{\delta x}$$

Left-handed difference quotients:

$$\frac{\partial}{\partial x_1} u(x_1, x_2, t) \approx \frac{u(x_1, x_2, t) - u(x_1 - \delta x, x_2, t)}{\delta x}$$

$$\frac{\partial}{\partial x_2} u(x_1, x_2, t) \approx \frac{u(x_1, x_2, t) - u(x_1, x_2 - \delta x, t)}{\delta x}$$

The Finite-Difference Method in Two Dimensions

Central difference quotients:

$$\frac{\partial}{\partial x_1} u(x_1, x_2, t) \approx \frac{u(x_1 + \delta x, x_2, t) - u(x_1 - \delta x, x_2, t)}{2\delta x}$$

$$\frac{\partial}{\partial x_1} u(x_1, x_2, t) \approx \frac{u(x_1 + \frac{\delta x}{2}, x_2, t) - u(x_1 - \frac{\delta x}{2}, x_2, t)}{\delta x}$$

$$\frac{\partial}{\partial x_2} u(x_1, x_2, t) \approx \frac{u(x_1, x_2 + \delta x, t) - u(x_1, x_2 - \delta x, t)}{2\delta x}$$

$$\frac{\partial}{\partial x_2} u(x_1, x_2, t) \approx \frac{u(x_1, x_2 + \frac{\delta x}{2}, t) - u(x_1, x_2 - \frac{\delta x}{2}, t)}{\delta x}$$

and all other variants discussed in the one-dimensional case

The Energy Balance

$$\frac{\partial}{\partial t} \epsilon(\vec{x}, t) = -\operatorname{div} \vec{q}(\vec{x}, t) + Q(\vec{x}, t)$$

where

$\epsilon(\vec{x}, t)$ = energy density [$\frac{\text{J}}{\text{m}^3}$]

$\vec{q}(\vec{x}, t)$ = heat flux density [$\frac{\text{W}}{\text{m}^2}$]

$Q(\vec{x}, t)$ = rate of production of thermal energy per volume [$\frac{\text{W}}{\text{m}^3}$]

The Specific Heat Capacity

The specific heat capacity

$$c = \frac{1}{\rho} \frac{\partial \epsilon}{\partial T}$$

describes the change in thermal energy with temperature.



$$\frac{\partial}{\partial t} \epsilon(\vec{x}, t) = \rho c \frac{\partial}{\partial t} T(\vec{x}, t) = -\operatorname{div} \vec{q}(\vec{x}, t) + Q(\vec{x}, t)$$

Water: $c = 4180 \frac{\text{J}}{\text{kgK}}$

Rocks: $c = 800\text{--}1000 \frac{\text{J}}{\text{kgK}}$

The Three Mechanisms of Heat Transport

Heat conduction: Driven by spatial differences in temperature.

Advective transport: Heat is carried by a moving (flowing) medium.

$$\vec{q}(\vec{x}, t) = \epsilon(\vec{x}, t) \vec{v} = \rho c T(\vec{x}, t) \vec{v}$$

Radiation: Does not require a medium, but is only significant at very high temperatures.

Fourier's Law of Heat Conduction (1822)

- 1 Heat flux follows the direction of steepest descent of the temperature field $T(\vec{x}, t)$.
- 2 The heat flux density is proportional to the decrease of temperature per length.

$$\vec{q}(\vec{x}, t) = -\lambda \nabla T(\vec{x}, t) = -\lambda \begin{pmatrix} \frac{\partial}{\partial x_1} T(\vec{x}, t) \\ \frac{\partial}{\partial x_2} T(\vec{x}, t) \\ \frac{\partial}{\partial x_3} T(\vec{x}, t) \end{pmatrix}$$

with

$$\lambda = \text{thermal conductivity} \left[\frac{\text{W}}{\text{mK}} \right]$$

Typical Values of λ

Material	λ [$\frac{W}{mK}$]
diamond	2300
iron	80
quartz	1.4
sand	0.6
expanded polystyrene	0.033
water	0.6
air	0.026

Rocks	λ [$\frac{W}{mK}$]
granite	2.8
basalt	2
dolomite	2.5
limestone	2.5
sandstone	2.5
shale	2
widely used value	2.5

The Full Heat Equation (conduction, advection, production)

Energy balance + Fourier's law + advective heat flux



$$\rho c \frac{\partial}{\partial t} T(\vec{x}, t) = \operatorname{div}(\lambda \nabla T(\vec{x}, t) - \rho c T(\vec{x}, t) \vec{v}) + Q$$

The Thermal Diffusivity

If ρ , c , and λ are constant (mass balance implies $\text{div} \vec{v} = 0$ then), the heat equation can be simplified to

$$\begin{aligned} \frac{\partial}{\partial t} T(\vec{x}, t) &= \kappa \Delta T(\vec{x}, t) - \vec{v} \cdot \nabla T(\vec{x}, t) + \frac{Q}{\rho c} \\ &= \kappa \left(\frac{\partial^2}{\partial x_1^2} T(\vec{x}, t) + \frac{\partial^2}{\partial x_2^2} T(\vec{x}, t) + \frac{\partial^2}{\partial x_3^2} T(\vec{x}, t) \right) \\ &\quad - \vec{v} \cdot \nabla T(\vec{x}, t) + \frac{Q}{\rho c} \end{aligned}$$

with the thermal diffusivity

$$\kappa = \frac{\lambda}{\rho c}$$

Water: $\kappa = 1.4 \times 10^{-7} \frac{\text{m}^2}{\text{s}}$

Rocks: $\kappa \approx 10^{-6} \frac{\text{m}^2}{\text{s}} \approx 30 \frac{\text{m}^2}{\text{a}}$

Boundary Conditions

Boundary conditions for a second-order (concerning space) differential equation concern the values or their derivatives (or a combination of both).

Dirichlet boundary conditions define the temperatures at the boundaries:

$$T(\vec{x}, t) = T_b$$

Interpretation: System is coupled to a big reservoir held at a given temperature.

Boundary Conditions

(Von) Neumann boundary conditions define the conductive heat flux density across the boundaries:

$$-\lambda \nabla T(\vec{x}, t) \cdot \vec{n} = q_b$$

where \vec{n} is the outer unit normal vector on the surface.

In 1D:

$$\pm \lambda \frac{\partial}{\partial x} T(x, t) = q_b$$

Homogeneous (von) Neumann boundary condition: $q_b = 0$



$$\nabla T(\vec{x}, t) \cdot \vec{n} = 0 \quad (2D/3D), \quad \frac{\partial}{\partial x} T(x, t) = 0 \quad (1D)$$

Boundary Conditions

Mixed boundary conditions define a combination of temperature and temperature gradient normal to the surface.

Examples:

- Total (conductive + advective) heat flux density across the boundary is given:

$$(-\lambda \nabla T(\vec{x}, t) + \rho c T(\vec{x}, t) \vec{v}) \cdot \vec{n} = q_b$$

- Radiating surface (without advection):

$$-\lambda \nabla T(\vec{x}, t) \cdot \vec{n} = \sigma T(\vec{x}, t)^4$$