

Geothermics and Geothermal Energy

Deep Open Geothermal Systems

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Steps of Conversion

Thermal energy → mechanical work: turbine; rather low efficiency due to thermodynamic limitation

Mechanical work → electricity: generator; high efficiency

The Thermodynamic Limitation (Carnot Cycle)

$$\delta S = \frac{\delta Q_h}{T_h} + \frac{\delta Q_c}{T_c} \geq 0 \quad (1)$$

where

δQ_h = thermal energy supplied to to the hot system
< 0 (from the geothermal reservoir into the turbine)

T_h = temperature of the hot system

δQ_c = thermal energy supplied to the cold system
> 0 (out of the turbine)

T_c = temperature of the cold system

The Thermodynamic Limitation (Carnot Cycle)

Mechanical work yielded by one cycle (conservation of energy):

$$\delta W = -(\delta Q_h + \delta Q_c) \leq -\delta Q_h \left(1 - \frac{T_c}{T_h}\right) = -\eta_{\max} \delta Q_h \quad (2)$$

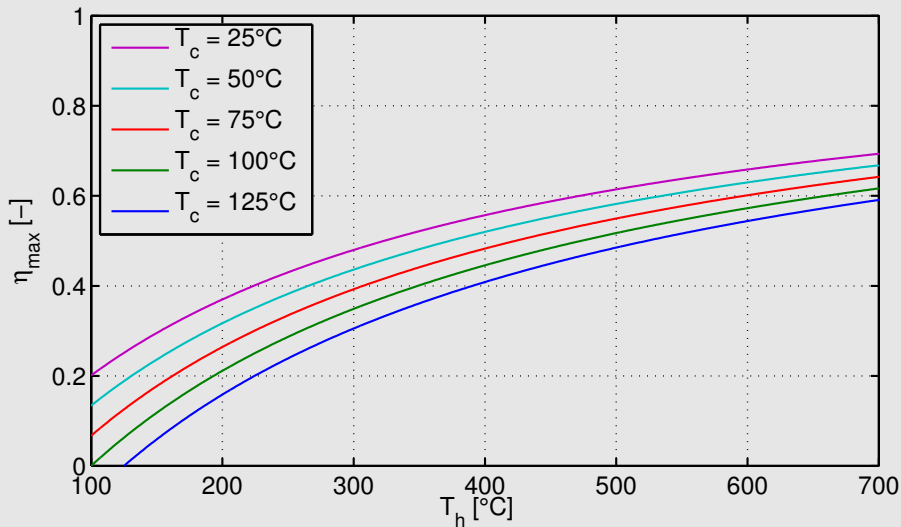
with the maximum efficiency

$$\eta_{\max} = \frac{T_h - T_c}{T_h} \quad (3)$$

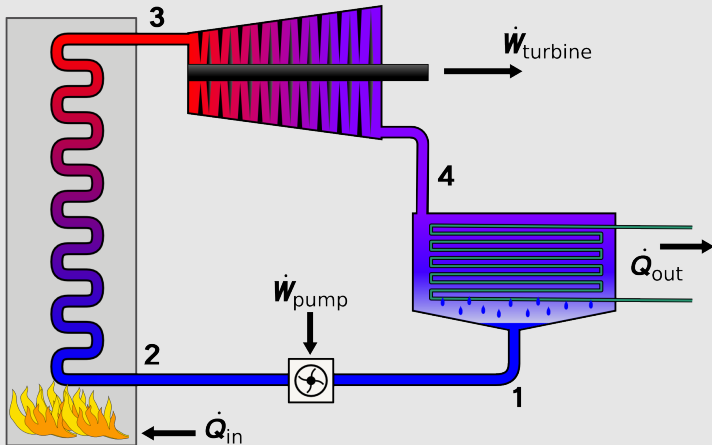
Consequence for the electrical, mechanical and thermal power of a geothermal power plant:

$$P_{\text{el}} < P_{\text{me}} < \eta_{\max} P_{\text{th}} \quad (4)$$

Maximum Efficiency of Converting Thermal Energy

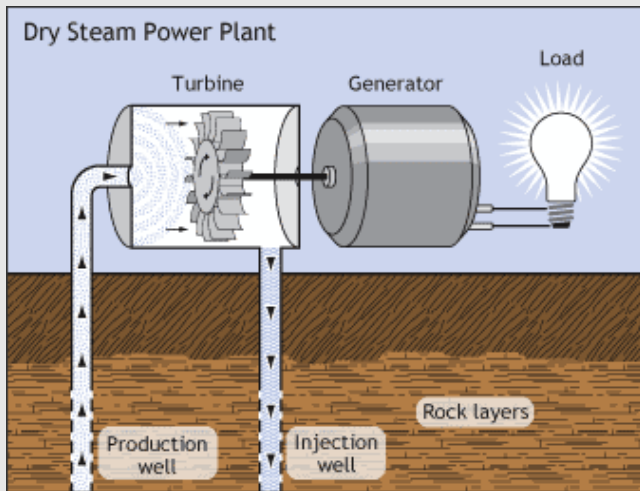


General Principle: Clausius-Rankine Cycle



Source: Wikipedia, © A. Ainsworth

Dry Steam Power Plants

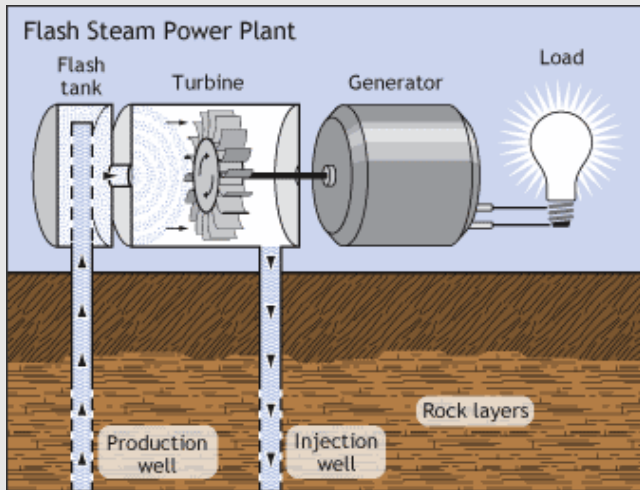


Source: Office of Energy Efficiency and Renewable Energy

Dry Steam Power Plants

- Rather simple technology
- First geothermal production of electricity: Larderello 1904
- Biggest geothermal power plant on Earth: “The Geysers”, California, USA, 750 MW_{el}
- Limited to few locations on Earth

Flash Steam Power Plants

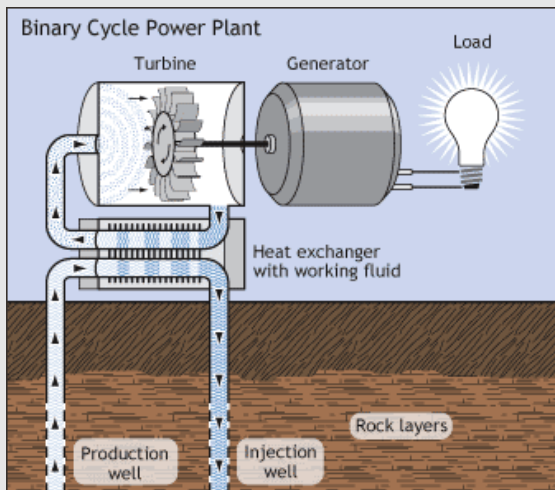


Source: Office of Energy Efficiency and Renewable Energy

Flash Steam Power Plants

- Most common type of geothermal power generation plants in operation today
- Reasonable efficiency only for high-enthalpy resources ($T > 200^{\circ}\text{C}$)

Binary Cycle Power Plants



Source: Office of Energy Efficiency and Renewable Energy

Binary Cycle Power Plants

- Heat transfer to a fluid with a boiling point below 100°C by a heat exchanger
- Applicable to low-enthalpy resources ($T < 200^{\circ}\text{C}$)
- Expensive technology
- Types:

Organic Rankine Cycle (ORC): Transfer heat to an organic fluid with a low boiling point and operate the turbine with this fluid, e. g., n-perfluoropentane (C_5F_{12} , boiling point 30°C , $T_c \approx 75^{\circ}\text{C}$)

Kalina cycle: Ammonia solution where the concentration of ammonia varies during the cycle; power plants in Germany at Unterhaching and Bruchsal

ORC Power Plants in Germany

Location	Depth [m]	T [°C]	Q [$\frac{1}{s}$]	P_{th} [MW]	P_{el} [MW]
Dürrnhaar	4114	130	135		5.5
Grünwald	4083	130	150	50	4.5
Insheim	3650	165	85		4.8
Kirchstockach	3750	139	145		5.5
Landau	3340	155	70		3.8
Neustadt-Glewe	2455	99	35	5.5	0.23
Sauerlach	4480	143	110		4.0
Simbach/Braunau	1942	80	74	7	0.2
Traunreut	4500	118	130		5.0 (?)

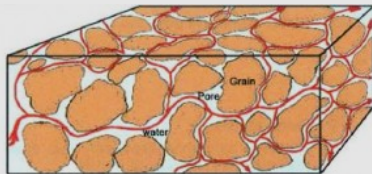
Kalina Cycle Power Plants in Germany

Location	Depth [m]	T [°C]	Q [$\frac{1}{s}$]	P_{th} [MW]	P_{el} [MW]
Unterhaching	3350	122	150	38	3.36*
Bruchsal	2542	120	24	5.5	0.55

* until 2017

Principle

- Hot water is extracted at one or more wells.
- Cold water is (re)injected at another well; in most cases at the same rate as total extraction.
- Flow of water through a porous rock.



Source: Borehole Wireline

Major Problem

Maintaining the fluid circulation in the rock consumes a considerable part of the produced energy.

Porosity of Rocks

Total porosity: $\phi = \frac{\text{void volume}}{\text{total volume}}$; $0 \leq \phi < 1$; often measured in percent

Effective porosity: only accessible pores and volume of water that can be extracted

Typical porosity values:

	ϕ_{tot} [%]	ϕ_{eff} [%]
equally sized spheres	26–48	26–48
soil	55	40
clay	50	2
sand	25	22
limestone	20	18
sandstone (semiconsolidated)	11	6
granite	0.1	0.09

Darcy's Law

- Empirically found by Henry Darcy (1856).
- Describes the average flow through a porous medium on macroscopic scales.
- Simplest form (without gravity):

$$\vec{v}(\vec{x}, t) = -\frac{k}{\eta} \nabla p(\vec{x}, t) \quad (5)$$

where

\vec{v} = volumetric flow rate (Darcy velocity) [$\frac{\text{m}}{\text{s}}$]

p = fluid pressure [Pa]

k = hydraulic permeability [m^2]

η = dynamic viscosity of the fluid [Pa s]

- Basically the same as Fourier's law of heat conduction.

The Hydraulic Permeability

- Units:

SI unit: m^2

Widely used unit: Darcy (D)

$$1 \text{ D} = 9.869 \times 10^{-13} \text{ m}^2 \approx 10^{-12} \text{ m}^2 = 1 \mu\text{m}^2$$

- $k = 1 \text{ D}$ results in a flow rate of $1 \frac{\text{cm}}{\text{s}}$ at a pressure drop of $1 \frac{\text{atm}}{\text{cm}}$ in water at 20°C ($\eta = 10^{-3} \text{ Pas}$).
- Typical values:

Medium	k [D]
gravel	10 – 1000
sand	0.01 – 10
silt	10^{-3} – 0.1

Medium	k [D]
limestone	10^{-6} – 100
fractured igneous rocks	10^{-6} – 10
unfractured igneous rocks	10^{-9} – 10^{-6}

The Darcy Equation

Balance equation for the mass of water per bulk volume

$$\frac{\partial \chi}{\partial t} = -\operatorname{div}(\rho_f \vec{v}) = \operatorname{div}\left(\rho_f \frac{k}{\eta} \nabla p\right) \quad (6)$$

where

χ = mass of fluid per bulk volume $[\frac{\text{kg}}{\text{m}^3}]$

ρ_f = fluid density $[\frac{\text{kg}}{\text{m}^3}]$



$$S \frac{\partial p}{\partial t} = -\operatorname{div}(\rho_f \vec{v}) = \operatorname{div}\left(\rho_f \frac{k}{\eta} \nabla p\right) \quad \text{with} \quad S = \frac{\partial \chi}{\partial p} \quad (7)$$

The Darcy Equation Compared to the Heat Conduction Equation

Basically the same equation as the heat conduction equation with a different meaning of the parameters.

heat conduction	T	λ	ρc	$\kappa = \frac{\lambda}{\rho c}$
Darcy flow	p	$\rho_f \frac{k}{\eta}$	S	$\tilde{\kappa} = \frac{\rho_f k}{\eta S}$

If all parameters are constant:

$$\frac{\partial T}{\partial t} = \kappa \Delta T, \quad \vec{q} = -\lambda \nabla T \quad (8)$$

$$\frac{\partial p}{\partial t} = \tilde{\kappa} \Delta p, \quad \vec{v} = -\frac{k}{\eta} \nabla p \quad (9)$$

Superposition of Solutions

The simplest form of Darcy's equation is linear.



Solutions can be superposed:

$$p(\vec{x}, t) = p_0(\vec{x}) + p_1(\vec{x}, t) + p_2(\vec{x}, t) + \dots \quad (10)$$

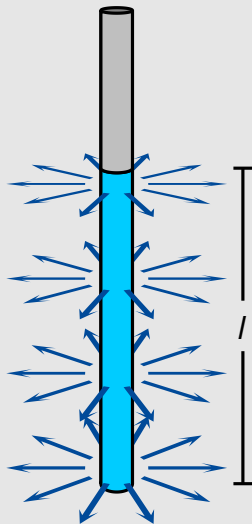
$$\vec{v}(\vec{x}, t) = \vec{v}_0(\vec{x}) + \vec{v}_1(\vec{x}, t) + \vec{v}_2(\vec{x}, t) + \dots \quad (11)$$

where

p_0, \vec{v}_0 = natural pressure and Darcy velocity without wells

p_i, \vec{v}_i = additional pressure and Darcy velocity caused by well # i

The Simplest Model for a Hydrothermal Well



Vertical borehole in an aquifer of a thickness l

Simplifications:

- All parameters (k , S , ρ_f , η) constant
- Only horizontal flow in radial direction



Basically the same solution as for the temperature drop of a downhole heat exchanger

Use variables p and \vec{v} for the additional pressure and Darcy velocity instead of p_i and \vec{v}_i .

The Simplest Model for a Hydrothermal Well

Downhole heat exchanger:

$$T(r, t) = -\frac{P_l}{4\pi\lambda} E_1\left(\frac{r^2}{4\kappa t}\right) \quad (12)$$

Hydrothermal well:

$$p(r, t) = \frac{\frac{\rho_f Q}{l}}{4\pi\rho_f\frac{k}{\eta}} E_1\left(\frac{r^2}{4\tilde{\kappa}t}\right) = \frac{\eta Q}{4\pi kl} E_1\left(\frac{r^2}{4\tilde{\kappa}t}\right) \quad (13)$$

where

$$Q = \text{rate of injection } \left[\frac{\text{m}^3}{\text{s}}\right], \quad Q < 0 \text{ for extraction}$$

Well Doublets

$\tilde{\kappa} \gtrsim 1 \frac{\text{m}^2}{\text{s}}$ for highly permeable rocks ($k \gtrsim 0.01 D$) required for hydrothermal systems if the rock is fully saturated with water.



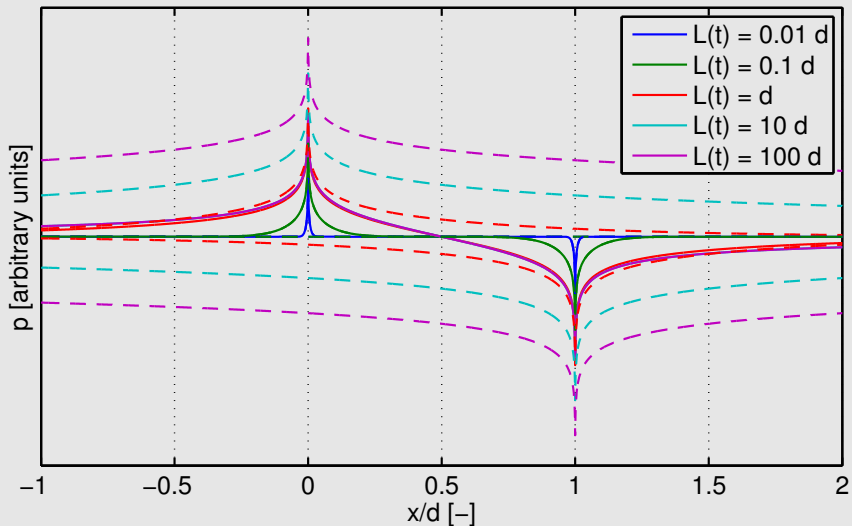
Pressure rapidly decreases around an extraction well.

Solution: Use a well doublet consisting of an injection well and an extraction well working at the same flow rate.

$$p(x, y, t) = \frac{\eta Q}{4\pi k l} \left(E_1 \left(\frac{r_i^2}{4\tilde{\kappa} t} \right) - E_1 \left(\frac{r_e^2}{4\tilde{\kappa} t} \right) \right) \quad (14)$$

where $r_{i/e}$ is the distance of the considered point from the injection / extraction well.

Pressure Distribution of a Well Doublet Compared to a Single Well



Well Doublets

Use the approximation

$$E_1(v) \approx -\ln(v) - 0.5772 \quad \text{for } v \ll 1 \quad (15)$$

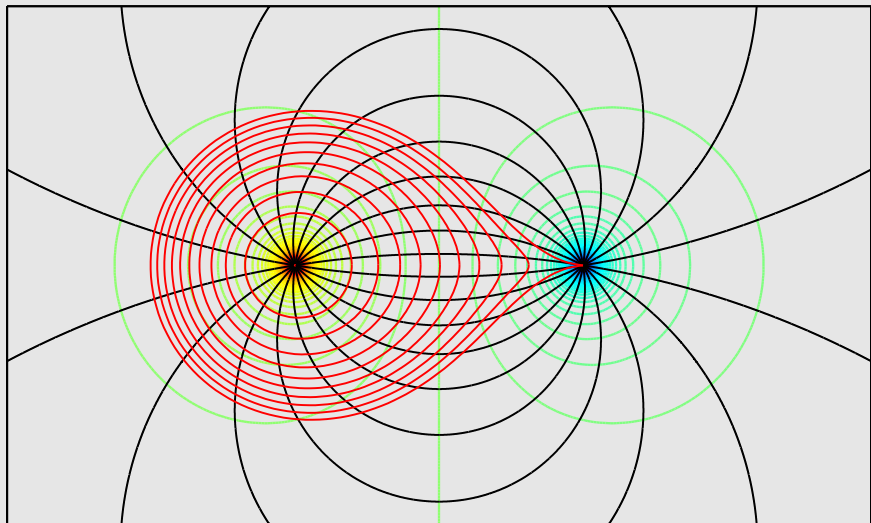


$$p(x, y, t) \approx \frac{\eta Q}{4\pi kl} \left(-\ln \left(\frac{r_i^2}{4\tilde{\kappa}t} \right) + \ln \left(\frac{r_e^2}{4\tilde{\kappa}t} \right) \right) \quad (16)$$

$$= \frac{\eta Q}{2\pi kl} \ln \frac{r_e}{r_i} \quad (17)$$

is independent of t (steady-state flow conditions).

Pressure and Flow Lines of a Simple Well Doublet



The Simplest Model for a Well Doublet

Limitation: In principle only valid

- for confined aquifers or
- if the horizontal distance of the wells is much smaller than the open borehole length l

Mechanical power required for maintaining the flow:

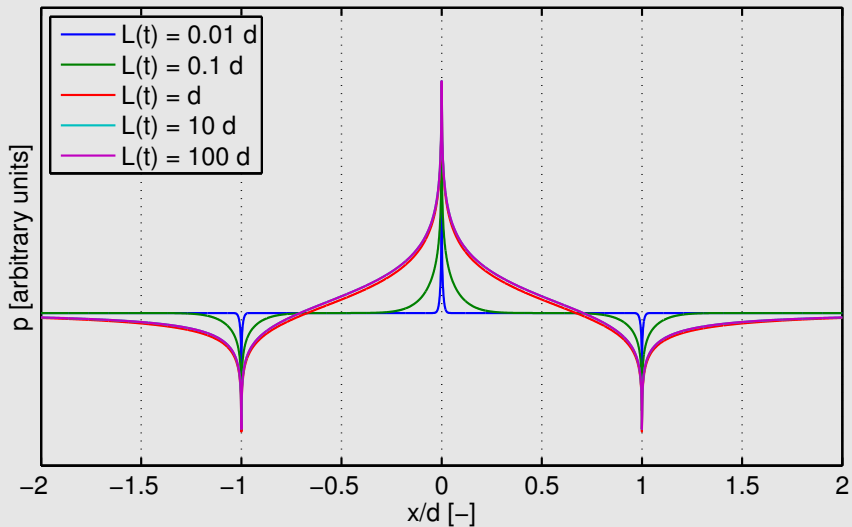
$$P = (p_i - p_e) Q \quad (18)$$

where

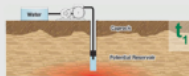
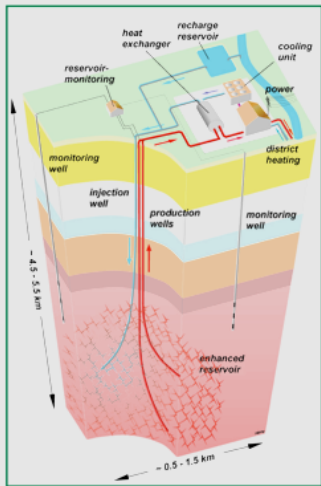
p_i = pressure at the walls of the injection well

p_e = pressure at the walls of the extraction well

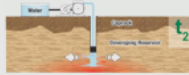
Well Triplet



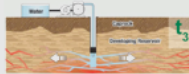
Hydraulic Fracturing for Increasing the Permeability



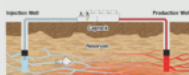
Drill a well to explore



Inject water to cause slip on faults (high water pressure pushes fractures open)



Injection extends a network of connected fractures



Inject water to sweep heat to a production well



Maximize production rate and lifetime

Source: NewEnergyNews

Environmental Issues related to Hydraulic Fracturing

- Large amounts of contaminated water if fracturing is supported by additional chemicals
- Fluid-induced seismicity

Mechanisms of Heat Transport in Porous Media

Solid matrix: conduction

Fluid: conduction and advection

Heat Exchange Between Fluid and Matrix

Length scale of heat conduction:

$$L(t) = \sqrt{\kappa t} \quad (19)$$

Water: $\kappa = 1.4 \times 10^{-7} \frac{\text{m}^2}{\text{s}}$

Rocks: $\kappa \approx 10^{-6} \frac{\text{m}^2}{\text{s}}$



Fluid and matrix rapidly adjust to the same temperature locally.

The Heat Equation for a Fluid

Heat flux density for a fluid moving at a velocity \vec{v} :

$$\vec{q} = \underbrace{-\lambda \nabla T}_{\text{conduction}} + \underbrace{\rho c T \vec{v}}_{\text{advection}} \quad (20)$$



$$\rho c \frac{\partial T}{\partial t} = -\text{div}(\vec{q}) \quad (21)$$

$$= \text{div}(\lambda \nabla T - \rho c T \vec{v}) \quad (22)$$

The Heat Equation for a Porous Medium

$$(\rho_m c_m + \phi \rho_f c_f) \frac{\partial T}{\partial t} = \operatorname{div}((\lambda_m + \phi \lambda_f) \nabla T - \rho_f c_f T \vec{v}) \quad (23)$$

where

- ρ_f, c_f, λ_f = parameters of the fluid
- ρ_m, c_m, λ_m = parameters of the dry matrix (not the solid!)
- ϕ = porosity
- \vec{v} = Darcy velocity



Effective velocity of heat advection:

$$\vec{v}_a = \frac{\rho_f c_f}{\rho_m c_m + \phi \rho_f c_f} \vec{v} \approx 1.7 \vec{v} \quad (24)$$

Velocities of Fluid Flow and Heat Transport

Mean interstitial velocity of the water particles

$$\vec{v}_p = \frac{\vec{v}}{\phi} \quad (25)$$

is significantly higher than the flow rate (Darcy velocity) \vec{v} .

Effective velocity of heat advection

$$\vec{v}_a = \frac{\rho_f c_f}{\rho_m c_m + \phi \rho_f c_f} \vec{v} \approx 1.7 \vec{v} \quad (26)$$

is also higher than the flow rate \vec{v} , but lower than the mean interstitial velocity \vec{v}_p .

Velocities of Fluid Flow and Heat Transport

$$\vec{v}_a = \frac{\phi \rho_f c_f}{\rho_m c_m + \phi \rho_f c_f} \vec{v}_p = \frac{\vec{v}_p}{R} \quad (27)$$

where

$$R = \frac{\rho_m c_m + \phi \rho_f c_f}{\phi \rho_f c_f} = 1 + \frac{\rho_m c_m}{\phi \rho_f c_f} \quad (28)$$

is the **coefficient of retardation**.



Water circulates R times between the wells until the cold temperature front breaks through (if heat conduction is neglected).