

Geothermics and Geothermal Energy

Deep Open Geothermal Systems

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Steps of Conversion

Thermal energy \rightarrow mechanical work: turbine;
rather low efficiency due to
thermodynamic limitation

Mechanical work \rightarrow electricity: generator; high
efficiency

Entropy



Source: Wehrli, Die Kunst aufzuräumen

Entropy

Definition of entropy:

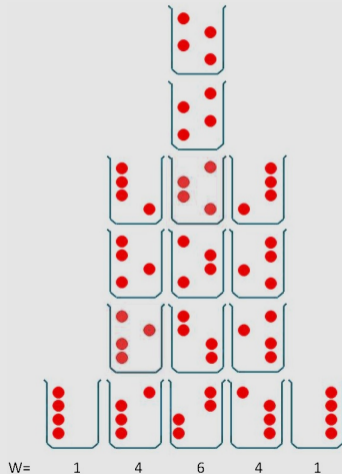
$$S = k \ln N \quad (1)$$

where

$$k = 1.38 \times 10^{-23} \frac{\text{J}}{\text{K}}$$

= Boltzmann constant

N = number of states that cannot be distinguished



Source: Wikipedia

Entropy

- Second law of thermodynamics: Entropy of a closed system cannot decrease through time.
- Processes where the entropy is constant are reversible.
- Relationship from classical thermodynamics: Adding an amount of thermal energy δQ at constant temperature T increases the entropy by

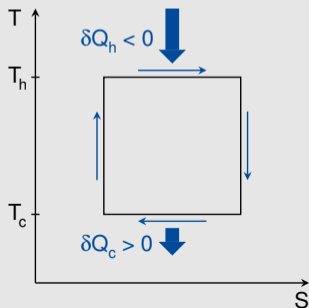
$$\delta S = \frac{\delta Q}{T} \quad (2)$$

or in integral form

$$\delta S = \int \frac{dQ}{T} \quad (3)$$

The Carnot Cycle

- Transfer of thermal energy from a “hot” reservoir (T_h) to a “cold” reservoir (T_c) yielding the maximum amount of mechanical work.
- Only a theoretical thermodynamic cycle, not a real physical process.
- Assumes two reservoirs of infinite capacity and a hypothetical gas.



Directions:

- isothermal expansion
(coupled to large reservoir)
- ← isothermal compression
(coupled to large reservoir)
- ↓ isentropic cooling
(by rapid expansion)
- ↑ isentropic heating
(by rapid compression)

The Thermodynamic Limitation of the Carnot Cycle

Total change in entropy after one cycle:

$$\delta S = \delta S_h + \delta S_c = \frac{\delta Q_h}{T_h} + \frac{\delta Q_c}{T_c} \geq 0 \quad (4)$$

where

δQ_h = thermal energy supplied to the hot system (< 0)

T_h = temperature of the hot system

δQ_c = thermal energy supplied to the cold system (> 0)

T_c = temperature of the cold system



$$\delta Q_c \geq -\delta Q_h \frac{T_c}{T_h} \quad (5)$$

Maximum Efficiency of Converting Thermal Energy

Mechanical work yielded by one Carnot cycle (conservation of energy):

$$\delta W = -(\delta Q_h + \delta Q_c) \leq -\delta Q_h \left(1 - \frac{T_c}{T_h}\right) = \eta_{\max} (-\delta Q_h) \quad (6)$$

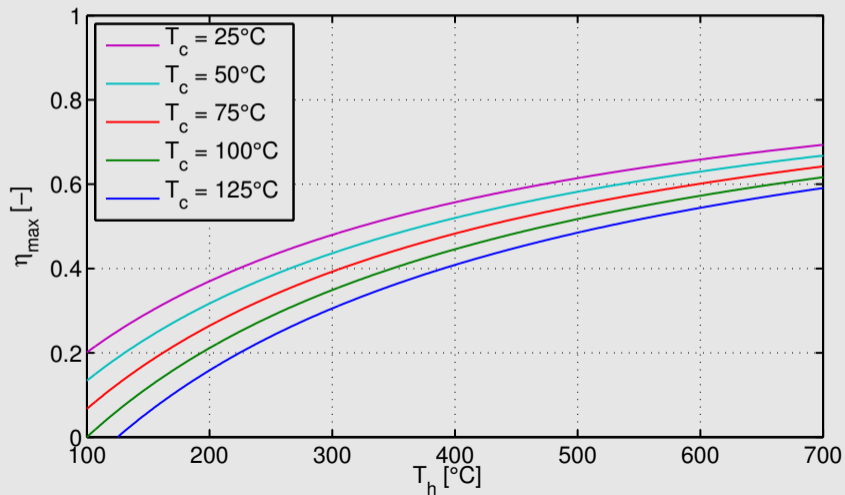
with the maximum efficiency

$$\eta_{\max} = \frac{T_h - T_c}{T_h} \quad (7)$$

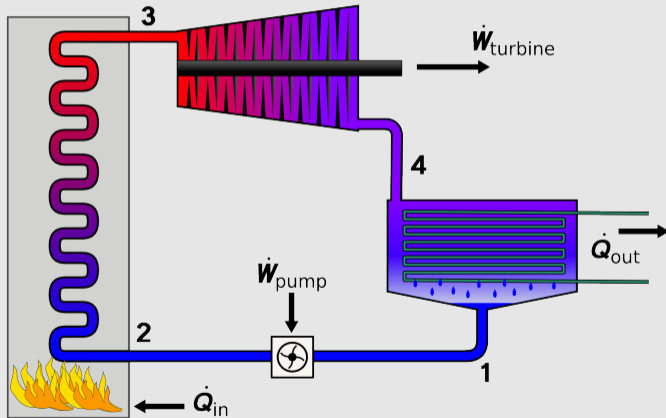
Consequence for the electrical, mechanical and thermal power of a geothermal power plant:

$$P_{\text{el}} < P_{\text{me}} < \eta_{\max} P_{\text{th}} \quad (8)$$

Maximum Efficiency of Converting Thermal Energy

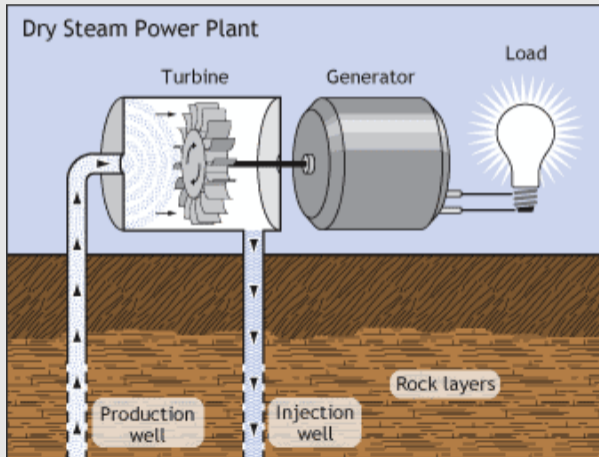


General Principle: Clausius-Rankine Cycle



Source: Wikipedia, © A. Ainsworth

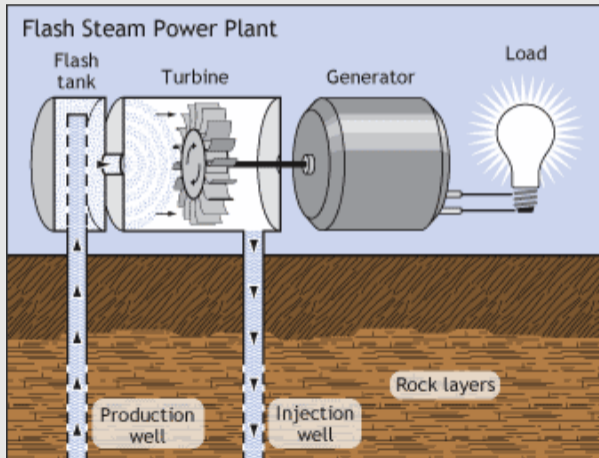
Dry Steam Power Plants



Source: Office of Energy Efficiency and Renewable Energy

- Rather simple technology
- First geothermal production of electricity: Larderello 1904
- Biggest geothermal power plant on Earth: "The Geysers", California, USA, 750 MW_{el}
- Limited to few locations on Earth

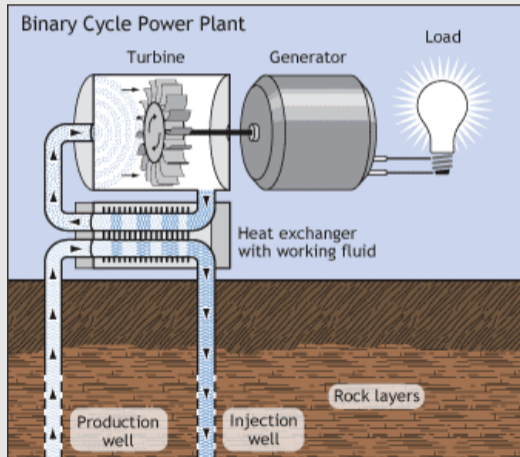
Flash Steam Power Plants



Source: Office of Energy Efficiency and Renewable Energy

- Most common type of geothermal power generation plants in operation today
- Reasonable efficiency only for high-enthalpy resources ($T > 200^{\circ}\text{C}$)

Binary Cycle Power Plants



Source: Office of Energy Efficiency and Renewable Energy

- Heat transfer to a fluid with a boiling point below 100°C by a heat exchanger
- Applicable to low-enthalpy resources ($T < 200^{\circ}\text{C}$)
- Expensive technology
- Types: Organic Rankine Cycle (ORC) and Kalina cycle

The Organic Rankine Cycle

Principle: Transfer heat to an organic fluid with a low boiling point and operate the turbine with the gas.

Fluids: various, e. g., n-perfluoropentane (C_5F_{12} , boiling point $30^\circ C$, $T_c \approx 75^\circ C$)

Technical challenges: not many; rather robust

Environmental issues: Some fluids act as greenhouse gases if released.

Installations in Germany: several

The Kalina Cycle

Development: in the 1970s by Aleksandr Kalina

Principle: Uses an ammonia (NH_3) solution in water; solubility decreases with temperature.



Separate ammonia from the solution at high temperature and operate the turbine with ammonia and then dissolve it at lower temperature.

Advantage: higher efficiency than ORC at low temperatures

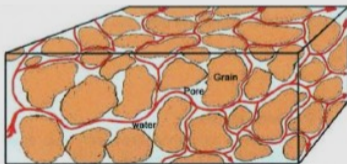
Technical challenges: several, in particular corrosion by ammonia and maintainance

Environmental issues: Ammonia is highly hazardous.

Installations in Germany: Unterhaching (2009–2017), Bruchsal, Taufkirchen

Principle

- Hot water is extracted at one or more wells.
- Cold water is (re)injected at another well; in most cases at the same rate as total extraction.
- Flow of water through a porous rock.



Source: Borehole Wireline

Porosity of Rocks

Total porosity: $\phi = \frac{\text{void volume}}{\text{total volume}}$; $0 \leq \phi < 1$; often measured in %

Effective porosity: only accessible pores and volume of water that can be extracted

	ϕ_{tot} [%]	ϕ_{eff} [%]
equally sized spheres	26–48	26–48
soil	55	40
clay	50	2
sand	25	22
limestone	20	18
sandstone (semiconsolidated)	11	6
granite	0.1	0.09

Source: GlobalSecurity.org

Darcy's Law

- Empirically found by Henry Darcy (1856).
- Describes the average flow through a porous medium on macroscopic scales.
- Simplest form (without gravity):

$$\vec{v}(\vec{x}, t) = -\frac{k}{\eta} \nabla p(\vec{x}, t) \quad (9)$$

where

\vec{v} = volumetric flux density (Darcy velocity) []

p = fluid pressure []

k = hydraulic permeability []

η = dynamic viscosity of the fluid []

Darcy's Law

- Basically the same as Fourier's law of heat conduction.
- With gravity almost the same, but p is the difference between pressure and hydrostatic pressure then.

The Hydraulic Permeability

SI unit: m^2

Widely used unit: Darcy (D)

$$1 \text{ D} = 9.869 \times 10^{-13} \text{ m}^2 \approx 10^{-12} \text{ m}^2 = 1 \mu\text{m}^2$$

$k = 1 \text{ D}$ results in a flow rate of $1 \frac{\text{cm}}{\text{s}}$ at a pressure drop of $1 \frac{\text{atm}}{\text{cm}}$ in water at 20°C ($\eta = 10^{-3} \text{ Pas}$).

Medium	k [D]	Medium	k [D]
gravel	10 – 1000	limestone	10^{-6} – 100
sand	0.01 – 10	fractured igneous rocks	10^{-6} – 10
silt	10^{-3} – 0.1	unfractured igneous rocks	10^{-9} – 10^{-6}

Darcy's Equation

Balance equation for the mass of water per bulk volume

$$\frac{\partial \chi}{\partial t} = -\operatorname{div}(\rho_f \vec{v}) = \operatorname{div}\left(\rho_f \frac{k}{\eta} \nabla p\right) \quad (10)$$

where

$$\chi = \text{mass of fluid per bulk volume } \left[\frac{\text{kg}}{\text{m}^3}\right]$$

$$\rho_f = \text{fluid density } \left[\frac{\text{kg}}{\text{m}^3}\right]$$



$$S \frac{\partial p}{\partial t} = -\operatorname{div}(\rho_f \vec{v}) = \operatorname{div}\left(\rho_f \frac{k}{\eta} \nabla p\right) \quad \text{with} \quad S = \frac{\partial \chi}{\partial p} \quad (11)$$

Darcy's Equation Compared to the Heat Conduction Equation

Basically the same equation as the heat conduction equation with a different meaning of the parameters.

heat conduction	T	λ	ρc	$\kappa = \frac{\lambda}{\rho c}$
Darcy flow	p	$\rho_f \frac{k}{\eta}$	S	$\tilde{\kappa} = \frac{\rho_f k}{\eta S}$

If all parameters are constant:

$$\frac{\partial T}{\partial t} = \kappa \Delta T, \quad \vec{q} = -\lambda \nabla T \quad (12)$$

$$\frac{\partial p}{\partial t} = \tilde{\kappa} \Delta p, \quad \vec{v} = -\frac{k}{\eta} \nabla p \quad (13)$$

Superposition of Solutions

The simplest form of Darcy's equation is linear.



Solutions can be superposed:

$$p(\vec{x}, t) = p_0(\vec{x}) + p_1(\vec{x}, t) + p_2(\vec{x}, t) + \dots \quad (14)$$

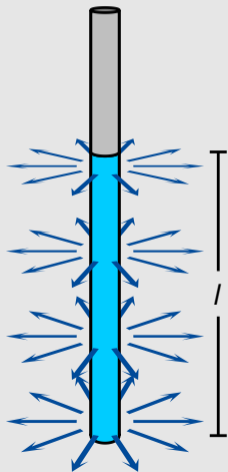
$$\vec{v}(\vec{x}, t) = \vec{v}_0(\vec{x}) + \vec{v}_1(\vec{x}, t) + \vec{v}_2(\vec{x}, t) + \dots \quad (15)$$

where

p_0, \vec{v}_0 = natural pressure and Darcy velocity without wells

p_i, \vec{v}_i = additional pressure and Darcy velocity caused by well i

The Simplest Model for a Hydrothermal Well



Vertical borehole in an aquifer of thickness l

Simplifications:

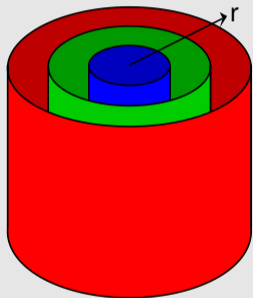
- All parameters (k , S , ρ_f , η) constant
- Only horizontal flow in radial direction



Widely used in hydrogeology for aquifer tests; introduced by C. V. Theis (1935).

Use variables p and \vec{v} for the additional pressure and Darcy velocity instead of p_i and \vec{v}_i .

Cylindrical Symmetry



Flow in radial direction requires that $p(x, y, z, t)$ only depends on $r = \sqrt{x^2 + y^2}$ and t ; use $p(r, t)$ instead of $p(x, y, z, t)$.



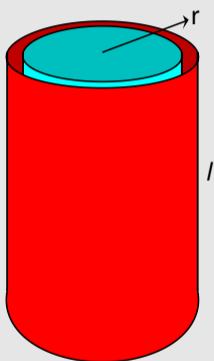
Darcy velocity

$$v(r, t) = -\frac{k}{\eta} \frac{\partial}{\partial r} p(r, t) \quad (16)$$

In other words (a bit sloppy):

$$\nabla = \frac{\partial}{\partial r} \quad (17)$$

Water Balance for a Cylindrical Shell



Change in mass of water m contained in the shell:

$$\begin{aligned}\frac{\partial m}{\partial t} &= (\pi r^2 l - \pi r^2 l) S \frac{\partial p}{\partial t} \\ &= 2\pi r l \rho_f v - 2\pi r l \rho_f v\end{aligned}\quad (18)$$



$$S \frac{\partial}{\partial t} p(r, t) = -\frac{1}{r} \frac{\partial}{\partial r} (r \rho_f v(r, t))\quad (19)$$

for $r - r \rightarrow 0$

In other words (a bit sloppy):

$$\text{div} = \frac{1}{r} \frac{\partial}{\partial r} r\quad (20)$$

Solution of Darcy's Equation for Cylindrical Symmetry

Insert (16) into (19):

$$S \frac{\partial}{\partial t} p(r, t) = \frac{1}{r} \frac{\partial}{\partial r} \left(r \rho_f \frac{k}{\eta} \frac{\partial}{\partial r} p(r, t) \right) \quad (21)$$

If all parameters are constant:

$$\frac{\partial}{\partial t} p(r, t) = \tilde{\kappa} \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial}{\partial r} p(r, t) \right) \quad (22)$$

with $\tilde{\kappa} = \frac{\rho_f k}{\eta S}$

Solution of Darcy's Equation for Cylindrical Symmetry

Rescaling approach already used for 1D heat conduction:

Define a nondimensional variable

$$u(r, t) = \frac{r}{2L(t)} = \frac{r}{2\sqrt{\tilde{k}t}} \quad (23)$$

and look for solutions where the shape of the pressure profile remains constant, while only the spatial scale changes.

Solution of Darcy's Equation for Cylindrical Symmetry

Solution for $p(r, t)$ with the conditions $p(r, 0) = 0$ and $p(r, t) \rightarrow 0$ for $r \rightarrow \infty$:

$$p(r, t) = -\frac{a}{2} E_1\left(\frac{r^2}{4\tilde{\kappa}t}\right) \quad (24)$$

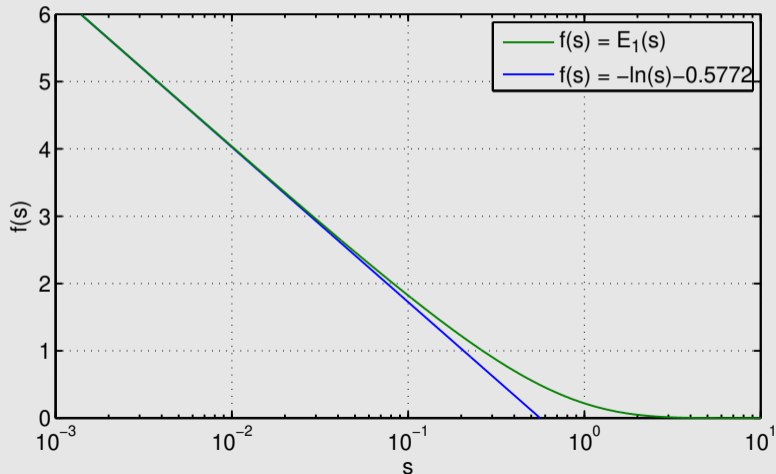
with the [exponential integral](#) function

$$E_1(s) = \int_s^{\infty} \frac{e^{-x}}{x} dx \quad (25)$$

and

$$a = \lim_{r \rightarrow 0} \left(r \frac{\partial}{\partial r} p(r, t) \right). \quad (26)$$

Solution of Darcy's Equation for Cylindrical Symmetry



Solution of Darcy's Equation for Cylindrical Symmetry

Total rate of injection through the walls of a thin cylinder (volume per time):

$$Q = \lim_{r \rightarrow 0} (2\pi r l v(r, t)) \quad (27)$$

$$= \lim_{r \rightarrow 0} \left(2\pi r l \left(-\frac{k}{\eta} \frac{\partial}{\partial r} p(r, t) \right) \right) \quad (28)$$

$$= -2\pi r l \frac{k}{\eta} a \quad (29)$$



$$p(r, t) = \frac{\eta}{4\pi k l} Q E_1 \left(\frac{r^2}{4\tilde{\kappa} t} \right) \quad (30)$$

Well Doublets

$\tilde{\kappa} \gtrsim 1 \frac{\text{m}^2}{\text{s}}$ for highly permeable rocks ($k \gtrsim 0.01 D$) required for hydrothermal systems if the rock is fully saturated with water.



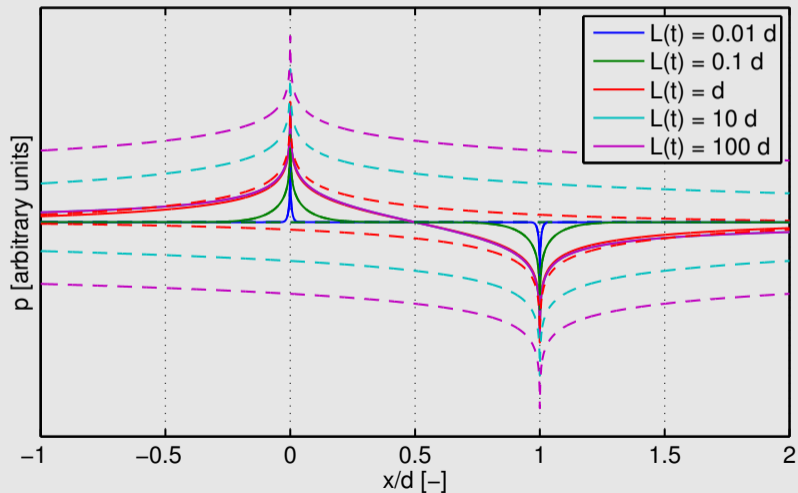
Pressure rapidly decreases around an extraction well.

Solution: Use a well doublet consisting of an injection well and an extraction well working at the same flow rate.

$$p(x, y, t) = \frac{\eta Q}{4\pi k l} \left(E_1 \left(\frac{r_i^2}{4\tilde{\kappa} t} \right) - E_1 \left(\frac{r_e^2}{4\tilde{\kappa} t} \right) \right) \quad (31)$$

where $r_{i/e}$ is the distance of the considered point from the injection / extraction well.

Pressure Distribution of a Well Doublet



Well Doublets

Use the approximation

$$E_1(s) \approx -\ln(s) - 0.5772 \quad \text{for } s \ll 1 \quad (32)$$

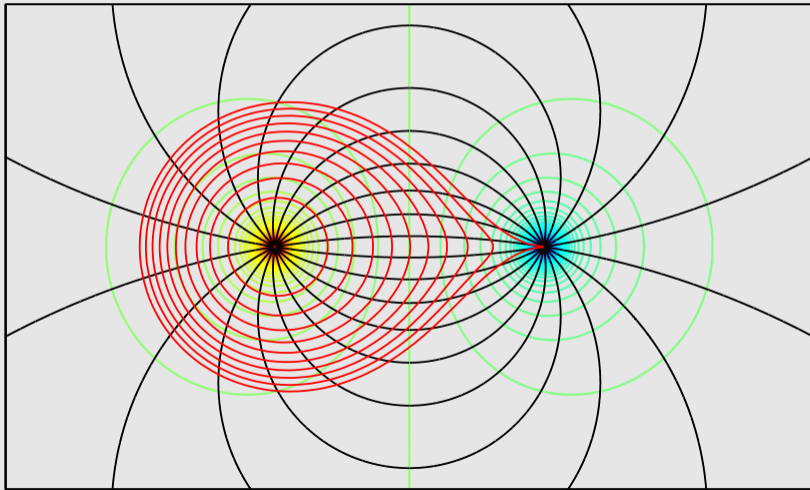


$$p(x, y, t) \approx \frac{\eta Q}{4\pi kl} \left(-\ln\left(\frac{r_i^2}{4\tilde{\kappa}t}\right) + \ln\left(\frac{r_e^2}{4\tilde{\kappa}t}\right) \right) \quad (33)$$

$$= \frac{\eta Q}{2\pi kl} \ln\left(\frac{r_e}{r_i}\right) \quad (34)$$

is independent of t (steady-state flow conditions).

Pressure and Flow Lines of a Simple Well Doublet



The Simplest Model for a Well Doublet

Limitation: In principle only valid

- for confined aquifers or
- if the horizontal distance of the wells is much smaller than the open borehole length l

Mechanical power required for maintaining the flow:

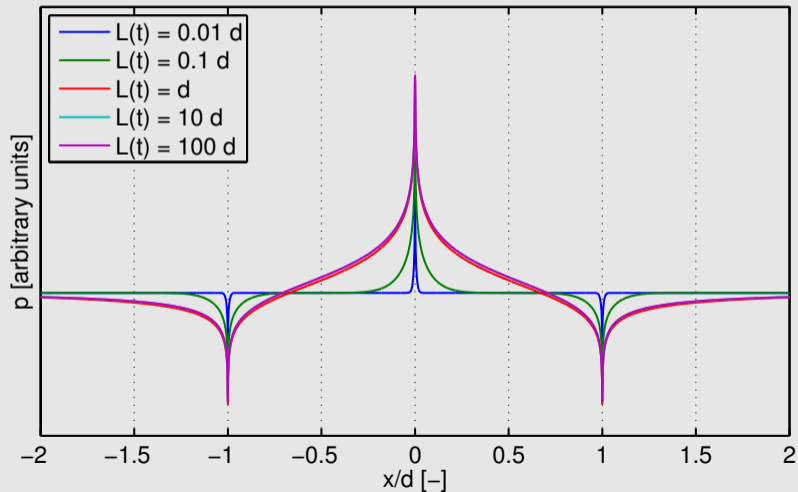
$$P = (p_i - p_e) Q \quad (35)$$

where

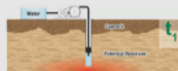
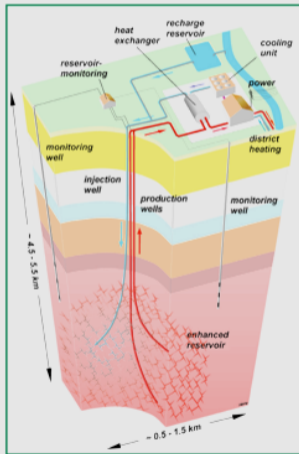
p_i = pressure at the walls of the injection well

p_e = pressure at the walls of the extraction well

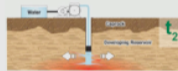
Well Triplet



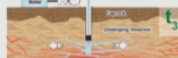
Hydraulic Fracturing for Increasing the Permeability



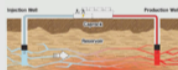
Drill a well to explore



Inject water to cause slip on faults (high water pressure pushes fractures open)



Injection extends a network of connected fractures



Inject water to sweep heat to a production well



Maximize production rate and lifetime

Source: NewEnergyNews

Hydraulic Fracturing for Increasing the Permeability

How to open existing fractures

- Fluid pressure
- Chemicals, e. g., 10–30 % HCl in carbonatic rocks

How to keep fractures open afterwards

- Proppant, e. g., sand
- Natural displacement

Environmental Issues related to Hydraulic Fracturing

- Large amounts of contaminated water if chemicals are used; may even get into contact with groundwater
- Fluid-induced seismicity

Mechanisms of Heat Transport in Porous Media

Solid matrix: conduction

Fluid: conduction and advection

Heat Exchange Between Fluid and Matrix

Length scale of heat conduction:

$$L(t) = \sqrt{\kappa t} \quad (36)$$

Water: $\kappa = 1.4 \times 10^{-7} \frac{\text{m}^2}{\text{s}}$

Rocks: $\kappa \approx 10^{-6} \frac{\text{m}^2}{\text{s}}$



Fluid and matrix rapidly adjust to the same temperature locally.

The Heat Equation for a Fluid

Heat flux density for a fluid moving at a velocity \vec{v} :

$$\vec{q} = \underbrace{-\lambda \nabla T}_{\text{conduction}} + \underbrace{\rho c T \vec{v}}_{\text{advection}} \quad (37)$$



$$\rho c \frac{\partial T}{\partial t} = -\text{div}(\vec{q}) \quad (38)$$

$$= \text{div}(\lambda \nabla T - \rho c T \vec{v}) \quad (39)$$

The Heat Equation for a Porous Medium

$$(\rho_m c_m + \phi \rho_f c_f) \frac{\partial T}{\partial t} = \operatorname{div}((\lambda_m + \phi \lambda_f) \nabla T - \rho_f c_f T \vec{v}) \quad (40)$$

where

ρ_f, c_f, λ_f = parameters of the fluid

ρ_m, c_m, λ_m = parameters of the dry matrix (not the solid!)

ϕ = porosity

\vec{v} = flux density (Darcy velocity)



Effective velocity of heat advection:

$$\vec{v}_a = \frac{\rho_f c_f}{\rho_m c_m + \phi \rho_f c_f} \vec{v} \approx \boxed{} \vec{v} \quad (41)$$

Velocities of Fluid Flow and Heat Transport

Mean interstitial velocity of the water particles

$$\vec{v}_p = \frac{\vec{v}}{\phi} \quad (42)$$

is significantly higher than the flux density (Darcy velocity) \vec{v} .

Effective velocity of heat advection

$$\vec{v}_a = \frac{\rho_f c_f}{\rho_m c_m + \phi \rho_f c_f} \vec{v} \approx 1.7 \vec{v} \quad (43)$$

is also higher than the flow rate \vec{v} , but lower than the mean interstitial velocity \vec{v}_p .

Velocities of Fluid Flow and Heat Transport

$$\vec{v}_a = \frac{\phi \rho_f c_f}{\rho_m c_m + \phi \rho_f c_f} \vec{v}_p = \frac{\vec{v}_p}{R} \quad (44)$$

where

$$R = \frac{\rho_m c_m + \phi \rho_f c_f}{\phi \rho_f c_f} = 1 + \frac{\rho_m c_m}{\phi \rho_f c_f} \quad (45)$$

is the **coefficient of retardation**.



Water circulates R times between the wells until the cold temperature front breaks through (if heat conduction is neglected).